## REMARKS

Attached hereto is a marked-up version of the changes made to the specification and claims by the current amendment. The attached page(s) is captioned "**Version With Markings To Show Changes Made**."

Respectfully submitted,

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## VERSION WITH MARKINGS TO SHOW CHANGES MADE

### IN THE CLAIMS

4. (Amended) A process as claimed in [any one of the preceding claims] claim 1 which the molar ratio of alkene to carboxylic acid produced in the oxidation reaction zone is in the range 10:1 to 1:10.

6. (Amended) A process as claimed in [any one of claims 2 to 3] claim 2 in which alkene and/or carboxylic acid is separately recovered from the oxidation reaction product or separately added to the second reaction zone.

7. (Amended) A process as claimed in [any one of claims 1 to 3] claim 1 in which the alkane is ethane, the corresponding alkene being ethylene and the corresponding carboxylic acid being acetic acid.

10. (Amended) A process according to claim 8 [or claim 9] and wherein the molar ratio of alkene to carboxylic acid produced in the oxidation reaction zone is in the range 0.8: 1 to 1.4:1.

11. (Amended) A process according to [any one of claims 1 to 3] claim 1 wherein the concentration of alkene fed to the oxidation reaction zone is from greater than 0 and up to and including 50 mol% of the total feed, including

recycles.

12. (Amended) A process according to [any one of claims 1 to 3] claim 1 wherein the concentration of water fed to the oxidation reaction zone is from 0 to 50 mol% inclusive of the total feed, including recycles.

13. (Amended) A process according to [any one of claims 1 to 3] wherein alkene and water are fed into the oxidation reaction zone.

14. (Amended) A process according to [any one of claims 1 to 3] claim 1 wherein the alkene and water are fed into the oxidation reaction zone in an alkene : water ratio of 1 to 0.1-250 by weight.

17. (Amended) A process according to [any one of claims 1 to 3] claim 1 in which the at least one catalyst in the oxidation reaction zone comprises molybdenum.

19. (Amended) A process according to [any one of claims 1 to 3] claim 1 in which the oxidation reaction is carried out at a temperature in the range 100 to 400 $^{0}$C

20. (Amended) A process according to [any one of claims 1 to 3] in

which the oxidation reaction is carried out at atmospheric or superatmospheric pressure

21. (Amended) A process according to [any one of claims 1 to 3] in which the oxidation reaction is carried out at a GHSV of 500-10,000 $hr^{-1}$.

22. (Amended) A process according to [any one of claims 1 to 3] <u>claim 1</u> wherein the product stream from the oxidation reaction zone also comprises carbon oxides in an amount of less than 15 mol%.

23. (Amended) A process according to [any one of claims 1 to 3] in which the alkane is ethane, the corresponding alkene is ethylene, the corresponding carboxylic acid is acetic acid and wherein ethylene and water are fed into the oxidation reaction zone in a ratio of 1 to 0.1-10 by weight, the molar ratio of ethylene to acetic acid produced is in the range 0.8: